A Novel Integrated Scheme for Stabilizing Biological Oxidation Process Performance in Treating Waste Gas Streams

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VOC: Volatile organic compounds

- Typical air contaminants found in waste gas stream
 - Environmental concern due to their toxicity
 - Serious health problems: cancer
 - Precursor of Ozone (O₃)
- Sources of VOCs
 - Chemical manufacturing
 - Dry cleaners,
 - Paint booths,
 - and other sources using solvent.

VOC Control Technology

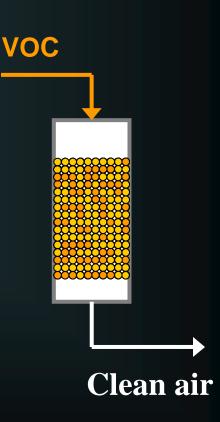
- Carbon adsorption,
- Liquid scrubbing,
- Condensation,
- Catalytic incineration,
- and Biological oxidation treatment.



Biological oxidation !!!

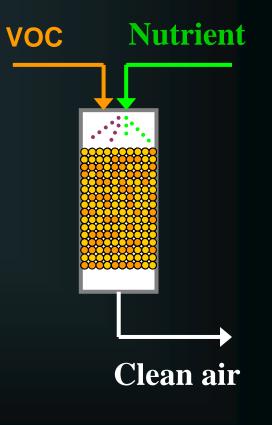
Biological Oxidation Process Biofiltration

- Typical biological oxidation process
- VOCs are removed through a biologically active media
- Natural organic media (soil, compost)
 → easily exhaust nutrient & buffer capacity
 → long term operation is not practical



Trickle Bed Air Biofilter (TBAB)

- Nutrient & buffer control
- Synthetic & inorganic media
 - → Optimizing the contaminant utilizing kinetics for microorganisms
 - → Long term, high removal performance



For more successful application in real industry
Load fluctuations

- Biofilter performance is best at steady loads of contaminants in waste stream
- Practically, waste streams in industry have
 - \rightarrow Variable airflow-rate
 - \rightarrow Variable VOC concentration
 - \rightarrow Non-use periods (e.g. weekend; holidays)



Solution = Buffer unit

Adsorption unit can be a buffer unit for a biofilter

Current application : Single bed of carbon filter

Problems of current adsorption unit
High loading & Large fluctuation → Losing buffer capacity
Initial period of operation → No contaminant to biofilter

Objective

Objective

Main Objective

A 2-bed adsorption unit is proposed to establish long-term stable buffer capacity of adsorption unit in mitigating biofilter performance

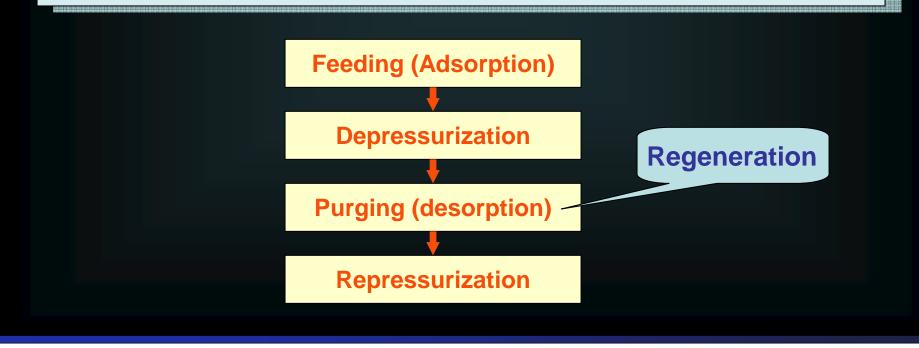
Specfic Objective

• To evaluate the overall performance of a integrated process scheme (2-bed adsorption unit + Biofilter)

• To be compared with that of a control unit without adsorption unit (Biofilter)

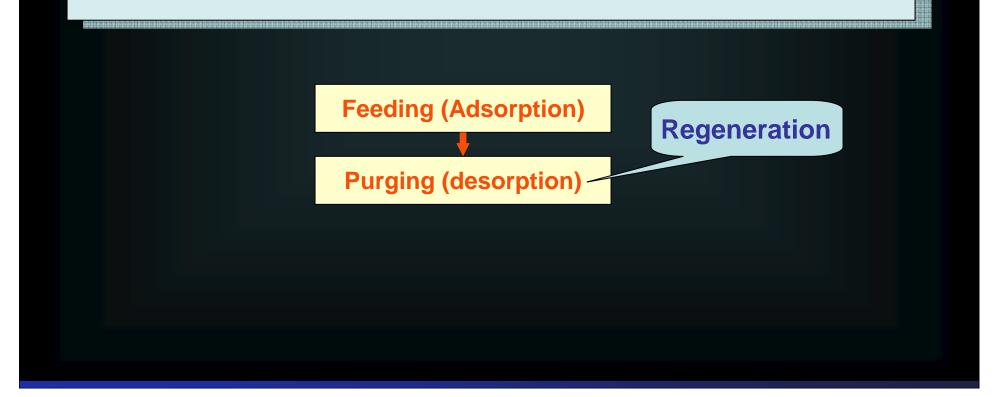
2-Bed Adsorption Unit

- Conceptually simple process to PSA
- PSA (Pressure Swing Adsorption) :
 - \rightarrow A technology for separation and purification for gas mixtures
 - \rightarrow 4 Steps for operational function



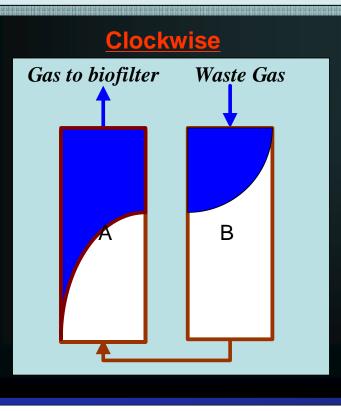
2-Bed Adsorption Unit

Hypothetically, if adsorption rate is equal to its desorption rate
 → Operational function is simplified to a 2-step

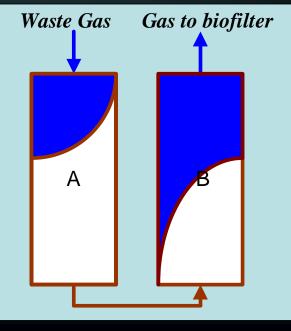


2-Bed Adsorption Unit

- Cyclic operation : Shift of air flow direction
 - \rightarrow Each bed will not be fully saturated with adsorbate



Counterclockwise



2-Bed Adsorption Unit

Will Serve as

- Polishing unit during the initial acclimation period of the biofilter
- Buffer unit in load fluctuation
- Feeding source without any feeding phase during non-use periods

Materials and Methods

Feeding Condition

Targeted VOC

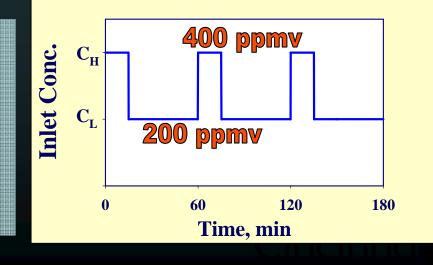
Toluene (C₇H₈)

- Common solvent employed in the industry
- A major component in paints and varnishes

Concentration & Loading

Square Wave Change

- Base = 200 ppmv
- Peak = 400 ppmv (15 mins / hour)
- Average concentration : 250 ppmv
- Average loading rate : 46.9 g/m³·hr



Feeding Condition

Targeted VOC

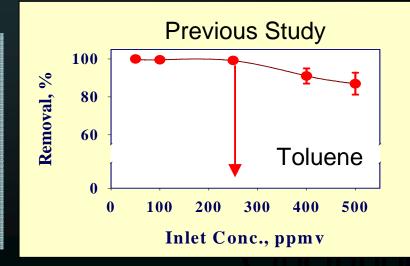
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Materials and Methods

Adsorption Unit

- 2 Beds
- Dimension : 2.5 cm (D) × 20 cm (L)
- Duration of one cycle : 8 hours
- EBRT: 5.6 sec (2.2 L/min)

• Absorbent : GAC (BPL 6 × 16 mesh)



Materials and Methods

Biofilter

Trickle Bed Air Biofilter (TBAB)

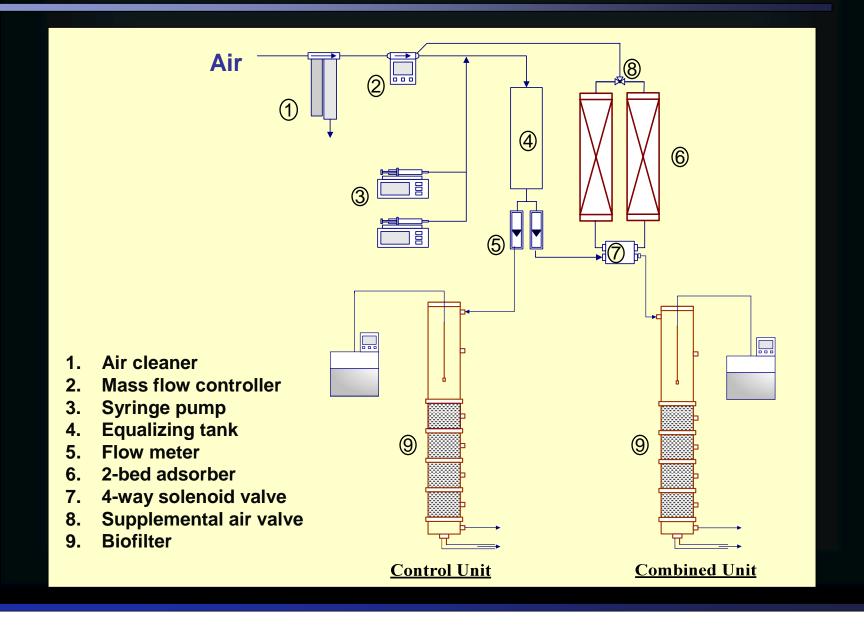
- Dimension : 76 mm (D) × 130 cm (L)
- Buffered nutrient solution supply
- Operating Temp. : 20 °C
- EBRT: 1.2 min (2.2L/min)

Media

- Celite[®] 6 mm R-635 Bio-Catalyst Carrier
- Packing depth : 60 cm
- Seeded with aerobic microbial culture pre-acclimating to toluene

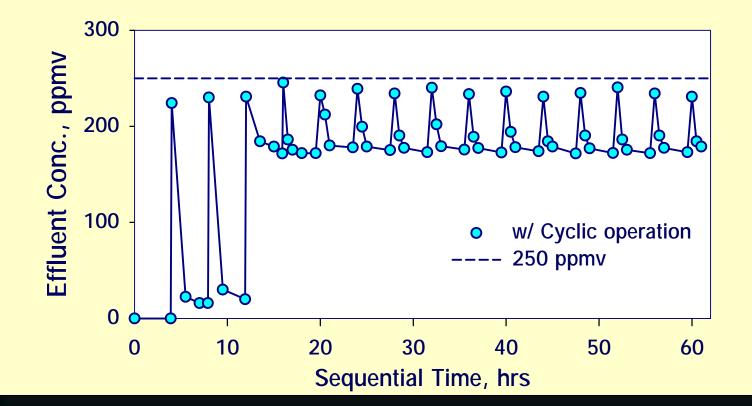


Schematic Diagram of Experimental Setup

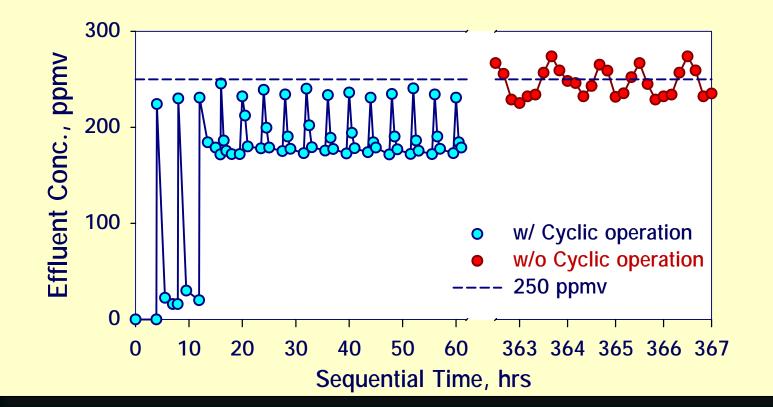


Experimental Results

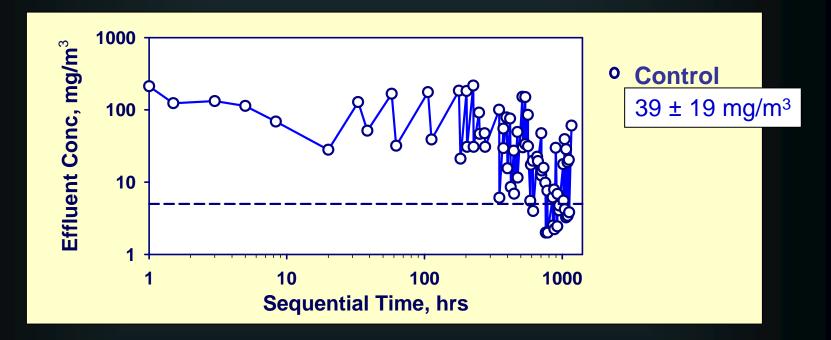
2-Bed Adsorption Performance



2-Bed Adsorption Performance

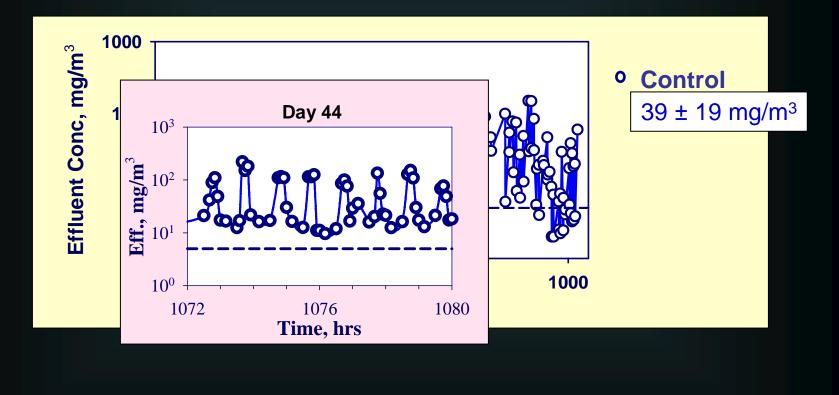


Effluent Concentration

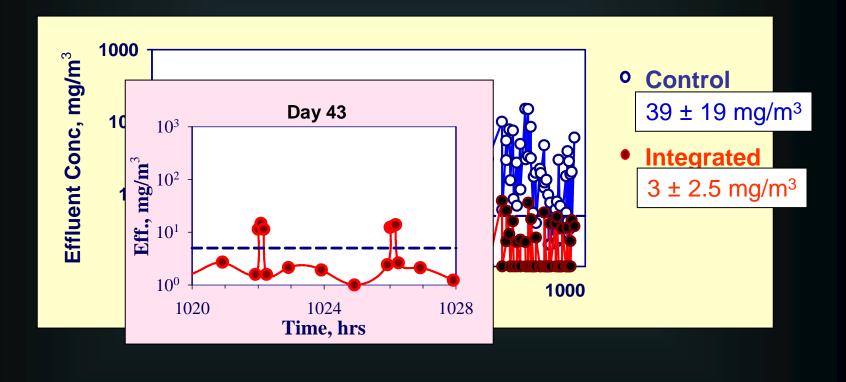


Exposure guideline (10 hrs average) : 5 mg/m³ (issued by American Industrial Hygiene Association)

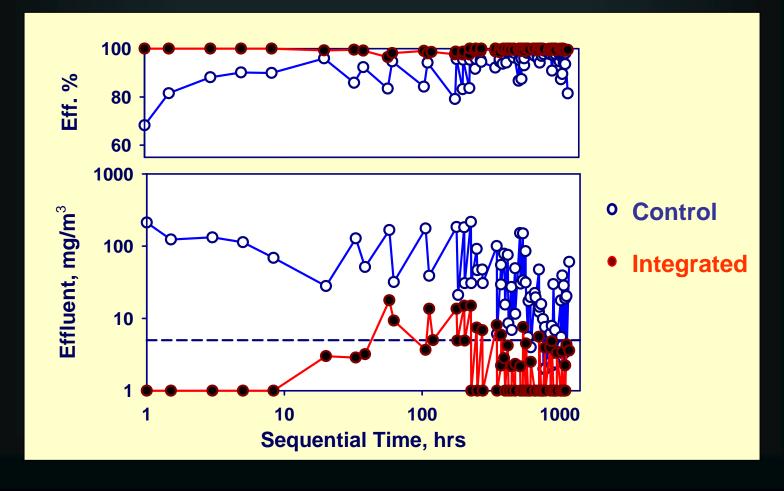
Effluent Concentration



Effluent Concentration



Removal Efficiency



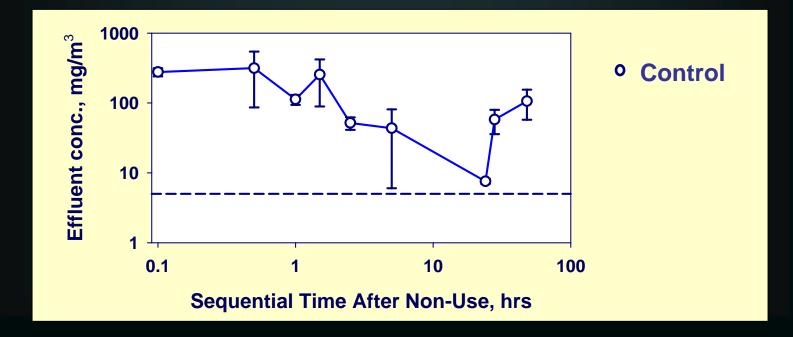
Effect of Non-Use Periods



Effect of Non-Use Periods

Reacclimation

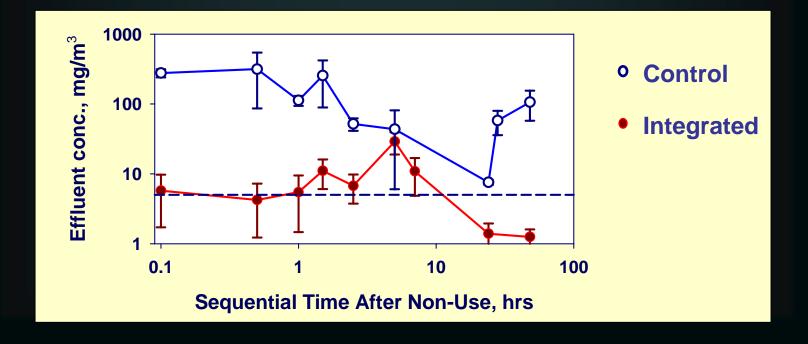
Effluent response after 2 days of starvation



Effect of Non-Use Periods

Reacclimation

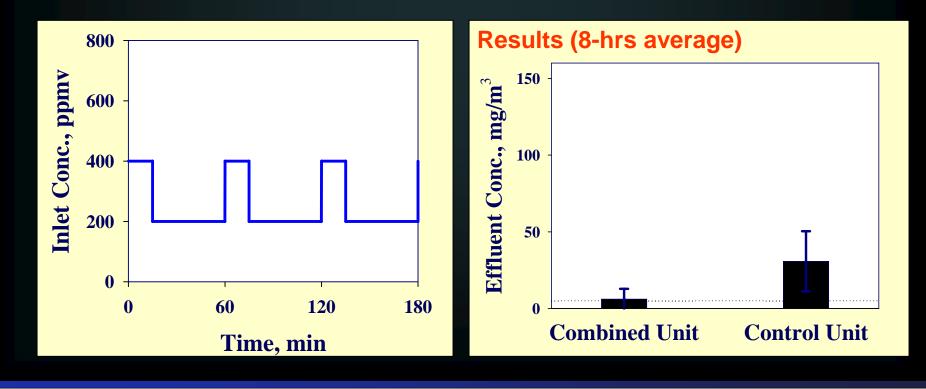
Effluent response after 2 days of starvation





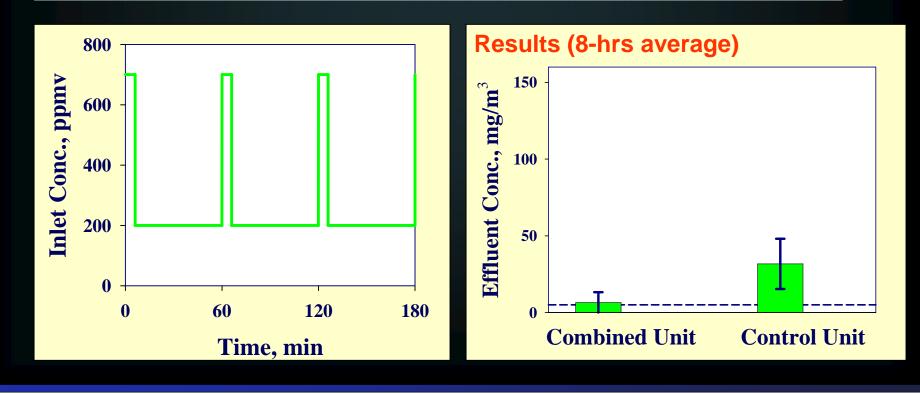
Feeding Conditions

• 1st : 46.9 g/m³·hr Peak: 400 ppmv for 15 mins Base: 200 ppmv for 45 mins



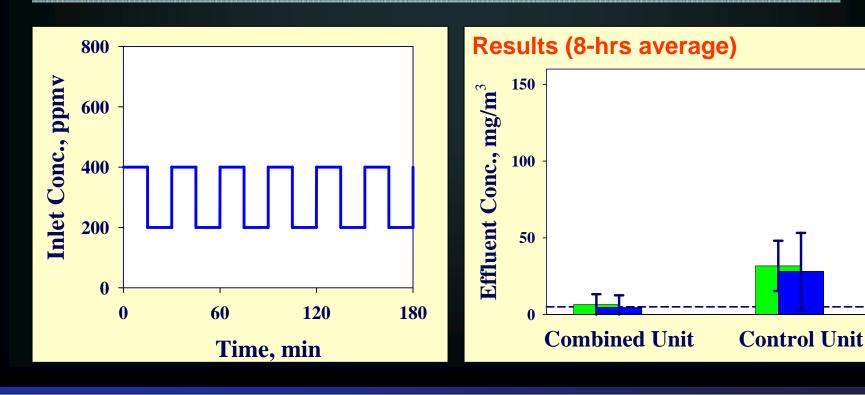
Feeding Condition

 2nd: High concentration of peak, 46.9 g/m³-hr Peak: 700 ppmv for 6 mins Base: 200 ppmv for 54 mins



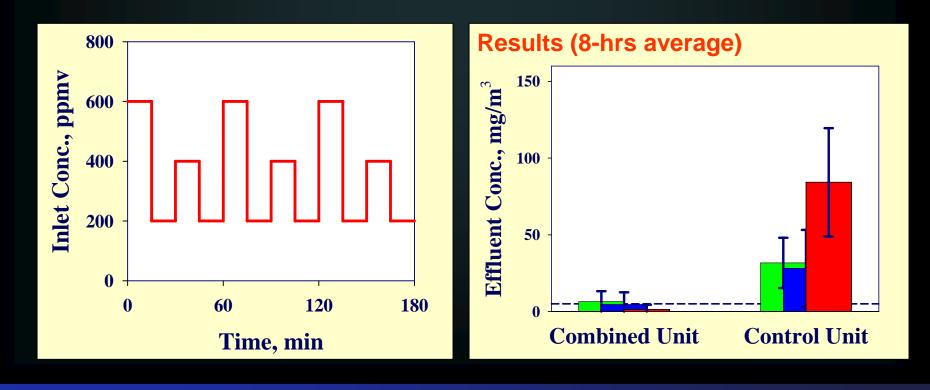
Feeding Condition

• 3rd : Frequent peak, 56.3 g/m³·hr Peak: 400 ppmv for 30 mins Base: 200 ppmv for 30 mins



Feeding Condition

 4th: High & Frequent peak, 65.9 g/m³-hr Peak: 600 ppmv for 15 mins & 400 ppmv for 15 mins Base: 200 ppmv



Conclusion

Conclusion

During unsteady-state loading conditions,

The 2-step of adsorption and desorption cycle in a 2-bed adsorption mitigated the adverse effect of load fluctuation on biofilter performance

The 2-Step cycle, i.e., adsorption and desorption, functioned as

- A polishing unit to abate the initial acclimation for the biofilter
- A buffering unit to dampen the biofilter performance
- A feeding source to the biofilter during non-use periods

